Subscripts

i component

Superscripts

saturation s

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Enthalpies of Formation, Densities, and Heat Capacities at 25 °C in the Liquid-Phase Region of the System $K_2O-P_2O_5-H_2O_5$

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Measurements of the enthalples of solution of monopotassium orthophosphate in various aqueous solutions of potassium hydroxide and phosphoric acid were made at 25 °C, and the apparent enthalples of formation of the solutions were derived. Measurements of the densities and heat capacities of the solutions also were made.

The heat requirements in the production of fertilizer solutions may be determined by measurement of the enthalpies of formation of solutions of different K2O:P2O5 ratios in the liquidphase region of the system $K_2O-P_2O_5-H_2O$. This information also would be helpful in determining both the enthalpies of hydrolysis of potassium polyphosphate solutions and the enthalpies of formation of solutions containing additional components such as ammonia, urea, and chloride.

Reported here are the results of measurements of the enthalpies of solution of KH2PO4 in various aqueous solutions of KOH and H_3PO_4 . The enthalpies of solution were combined with published values of enthalpies of formation to determine the enthalpies of formation of the solutions. The densities and the heat capacities of the solutions also are reported. Enthalpies of solution of $H_3PO_4(1)$, $KH_2PO_4(2)$, and $K_2HPO_4(3)$ have been reported. These data may be combined with published values of the enthalpies of formation of H_3PO_4 100 H_2O (4), KH_2PO_4 , and K₂HPO₄ (5) to derive the enthalpies of formation of orthophosphate solutions with mole ratios of K₂O:P₂O₅ of 0, 1, and 2.

Materials and Apparatus

Monopotassium orthophosphate was prepared by recrystallizing the reagent-grade salt from distilled water and drying at 105 °C. Chemical analyses showed this salt to contain 52.1% P2O5 and 34.6% K2O (stoichiometric; 52.15% P2O5, 34.61% K₂O). The potassium hydroxide solutions were prepared from reagent-grade KOH and distilled water. Their concentrations, expressed in molality (m_1) , were determined by acid titrations. The phosphoric acid solutions were prepared from reagent-grade H₃PO₄ and distilled water. Their concentrations, also expressed in molality (m_2) , were determined by chemical analyses.

The solution calorimeter, the method of measurement, and the corrections applied have been described (6, 7). The defined calorie was taken as 4.1840 absolute J. The average temperature for each of the solution periods is listed in the supplementary material (see paragraph at end of text regarding supplementary material). No corrections were applied to convert the enthalpies of solution to 25.00 °C.

Enthalpies of Solution of KH₂PO₄ in KOH Solutions

Monopotassium orthophosphate was added to each of the KOH solutions in successive increments to a final concentration near the saturation isotherm (8). The maximum temperature change during the solution period was arbitrarily set at about 1 °C, which limited the amount of solute to about 8 g at the lower concentrations of KH₂PO₄. The bulb volumes limited the amount of solute at the higher concentrations. The transfer of the final solution of one measurement from the calorimeter to a weighed fixed volume for the next measurement entailed some loss of the solution. Where larger amounts of solute were dissolved, there was still an excess of solution after the transfer and the excess could be removed before weighing the initial solution for the next measurement. Where smaller amounts of solute were dissolved, however, it was necessary to weigh the transferred solution and then add a weighed amount of the solvent (the KOH solution) to maintain the fixed volume. The concentration of the initial solution for the measurement thus could be determined. The concentration for each measurement, expressed as molality of KH_2PO_4 (m_2), is the average concentration of the initial and final solutions. The differential enthalpy of solution for each measurement was calculated from the equation

$$dT/dm_2 = 136.08934Q/1000w$$
(1)

where Q is the observed enthalpy change in calories, w is the

Table L	Coefficients	of Eq 2	for	KOH	Solvents
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			SD kcal (mol of			
m_1	m ₂	A	В	С	D	$KH_2PO_4)^{-1}$
0.506	0.000-0.492		tabular i	ntegration		
0.506	0.492-1.570	3.935	-0.109			0.01
0.998	0.000-0.945		tabular i	ntegration		
0.998	0.945-2.684	4.317	-1.472	0.8957	-0.1760	0.01
1.495	0.000-0.500	-16.103				0.04
1.495	0.500-1.379		tabular i	ntegration		
1.495	1.379-3.032	0.432	3.814	-1.6306	0.2321	0.01
1.987	0.000-0.600	-16.141	-0.170	-0.3105		0.02
1.987	0.600-1.788		tabular i	ntegration		
1.987	1.788-3.406	3.056	0.082			0.02
3.029	0.000-1.060	-16.209	0.247			0.05
3.029	1.060-1.700		tabular i	ntegration		
3.029	1.700-2.589	-1.263	0.139	-		0.00
3.029	2.589-4.217	0.907	1.147	-0.1385		0.02
4.121	0.000-1.400	-16.276	-0.216			0.05
4.121	1.400-2.000		tabular i	ntegration		
4.121	2.000-3.347	-2.020	0.371			0.02
4.121	3.347-5.138	5.471	3.379	-0.4037		0.11
4.645	0.000-1.560	-16.273	-0.256			0.03
4.645	1.560-2.180		tabular i	ntegration		
4.645	2.180-3.685	-2.432	0.476	-		0.02
4.645	3.685-5.691	-7.695	4.345	-0.4235		0.15

Table II. Coefficients for Eq 4

	coeff											
	A	В	С	D	E	F	SD					
R < 1	-5.996	1.997×10^{-1}	14.038	-4.716×10^{-3}	-8.832×10^{-1}	-2.393×10^{-2}	0.06					
1 < R < 2	-3.087	4.317×10^{-1}	9.980	-12.483×10^{-3}	-4.546×10^{-1}	-8.958×10^{-2}	0.14					
R > 2	15.572	$1.060 imes 10^{-1}$	4.784×10^{-2}	-4.303×10^{-3}	-1.287×10^{-3}	$8.238 imes10^{-3}$	0.07					

weight of KH_2PO_4 in grams dissolved during the measurement, and T is the total enthalpy change in kilocalories when m_2 mol of KH_2PO_4 is dissolved in 1000 g of the solvent. The gram formula weight of KH_2PO_4 is 136.08934. The measured values and the differential enthalpy of solution (dT/dm_2) for each measurement are listed in the supplementary material. The exothermic differential enthalpies of solution decrease rapidly in the concentration range equivalent to K_3PO_4 in water and change to endothermic at the concentration equivalent to K_2HPO_4 in water. Where it was convenient, the observed differential enthalpies of solution as a function of molality were fitted to equations of the form

$$dT/dm_2 = A + Bm_2 + Cm_2^2 + Dm_2^3$$
 (2)

for each solvent by the least-squares method. The coefficients of the equations for each of the solvents, along with their standard deviations and the concentration ranges in which they are effective, are listed in Table I. Integration of these equations with respect to m_2 plus the correct values for the integration constants and then division by m_2 gives the integral enthalpies of solution, ΔH , in kcal (mol of KH₂PO₄)⁻¹ as a function of molality. Where the differential enthalpies of solution change greatly with concentration, smooth curves were fitted to the observed values. Tabular integration and division by m_2 gave the integral enthalpies of solution at even values of m_2 in those concentration ranges. The ranges in which tabular integration was employed also are listed in Table I. The integral of eq 2 for each solvent and range of m_2 was solved for ΔH at the values of m_2 corresponding to integers of percent P₂O₅. In the ranges where tabular integration was employed, the values for ΔH were determined by straight-line interpolation between adjacent even values of m_2 . Values for percent K₂O corresponding to the integers of percent P2O5 were calculated from straight-line equations through percent K₂O in the solvent and percent P_2O_5 and percent K_2O and KH_2PO_4 . The equations for percent K2O as a function of percent P2O5, along with values of m_2 , ΔH , and percent K₂O corresponding to each integer of

percent P2O5, are listed in the supplementary material.

As stated earlier, the differential enthalpies of solution and thus the slopes of the integral enthalpies of solution change markedly at concentrations where the mole ratio of KOH:KH₂-PO₄ is 1 and 2, corresponding to K₂HPO₄ in water and K₃PO₄ in water, respectively. The mole ratio of KOH:KH₂PO₄, *R*, for each integer of percent P₂O₅ listed in the supplementary material was calculated from the equation

$$R = 1.50679(\% K_2 O / \% P_2 O_5) - 1$$
(3)

where 1.50679 is the gram formula weight ratio P_2O_5 :K₂O. These values for *R* also are listed in the supplementary material. Equations of the form

$$-\Delta H = A + BP + CR + DP^2 + ER^2 + FRP \qquad (4)$$

where *P* is the percent P₂O₅, were fitted to the values of *P*, *R*, and ΔH by the least-squares method over three ranges of *R* (*R* < 1, 1 < *R* < 2, and *R* > 2). The coefficients of the equations, the standard deviations, and the range of *R* for which each equation is effective are listed in Table II. Values for ΔH calculated from these equations also are listed in the supplementary material.

Enthalpy of Solution of KH₂PO₄ in H₃PO₄ Solutions

The procedure for determining the enthalpies of solution of KH_2PO_4 in H_3PO_4 solutions was similar to that described for KOH solutions, and eq 1 was used to determine the differential enthalpy of solution for each measurement (supplementary material).

Equation 2 was fitted to the observed differential enthalpies of solution as a function of solute molality for each solvent. The coefficients for eq 2 for each of the solvents, along with their standard deviations, are listed in Table III. Integration of these equations with respect to m_2 (the integration constant is zero in each case) and division by m_2 gives the integral en-

Table III. Coefficients of Eq 2 for H₃PO₄ Solvents

<i>m</i> ,	 	coeff A B C D								
 0.510	5 200	2 1 0 0	1 202	0.04(0	0.05					
0.510	5.209	-2.108	1.383	-0.3463	0.05					
1.019	5.151	-2.046	1.364	-0.3522	0.02					
1.514	5.100	-1.849	1.068	-0.2383	0.02					
1.988	5.031	-1.666	0.888	-0.1858	0.02					
3.076	4.484	-1.317	0.582	-0.1048	0.01					
4.106	4.658	-1.123	0.445	-0.0735	0.01					
5.081	4.474	-0.967	0.368	-0.0566	0.01					

thalpies of solution in kcal (mol of KH_2PO_4)⁻¹ as a function of molality. The integral of eq 2 for each solvent was solved for ΔH at the values of m_2 corresponding to integers of percent K₂O. Values for percent P₂O₅ corresponding to the integers of percent K₂O were calculated from straight-line equations through percent P₂O₅ in the solvent and percent P₂O₅ and percent K₂O in KH₂PO₄. The equations for percent P₂O₅ as a function of percent K₂O, along with values of m_2 , ΔH , and percent P₂O₅ corresponding to each integer of percent K₂O, are listed in Table IV. The equation

$$\Delta H = 5.110 - 0.1619K + 0.003195P + 0.002053K^2 - 0.001183P^2 + 0.003722PK$$
(5)

where K is percent K₂O and P is percent P₂O₅, fits the values calculated from the integrals of eq 2, with a standard deviation of 0.02 kcal (mol of KH₂PO₄)⁻¹. Values for ΔH calculated from eq 5 also are listed in Table IV.

Enthalpy of Formation of K2O-P2O5-H2O Solutions

The solution of KH_2PO_4 in KOH solutions can be described by the equation

$$\begin{aligned} \mathsf{KH}_2\mathsf{PO}_4 + R(\mathsf{KOH} \cdot x \mathsf{H}_2\mathsf{O}) &= \\ \mathsf{K}_2\mathsf{HPO}_4 \cdot (R - 1)\mathsf{KOH} \cdot (Rx + 1)\mathsf{H}_2\mathsf{O} \end{aligned} (6)$$

where R > 1 and by the equation

$$\begin{array}{l} \mathsf{KH}_{2}\mathsf{PO}_{4} + R(\mathsf{KOH} \cdot x \mathsf{H}_{2}\mathsf{O}) = \\ R(\mathsf{K}_{2}\mathsf{HPO}_{4}) \cdot (Rx + R)\mathsf{H}_{2}\mathsf{O} \cdot (R - 1)\mathsf{KH}_{2}\mathsf{PO}_{4} \end{array} (7)$$

where R < 1. The enthalpies of formation of the resultant solutions, $\Delta H_{\rm f}^{0}({\rm soln})$, in kcal (mol of ${\rm P_2O_5})^{-1}$, can be determined from the equation

$$\Delta H_{t}^{\circ}(\text{soln}) = 2[R\{\Delta H_{t}^{\circ}(\text{KOH} \times \text{H}_{2}\text{O})\} + \Delta H_{t}^{\circ}(\text{KH}_{2}\text{PO}_{4}) - \Delta H_{t}^{\circ}(\text{H}_{2}\text{O}) + \Delta H_{6}] (8)$$

where R > 1 and ΔH_6 is the integral enthalpy of solution for reaction 6 and from the equation

$$\Delta H_t^{\circ}(\text{soln}) = 2[R\{\Delta H_t^{\circ}(\text{KOH} \cdot x H_2 \text{O}) - \Delta H_t^{\circ}(\text{H}_2 \text{O})\} + \Delta H_t^{\circ}(\text{KH}_2 \text{PO}_4) + \Delta H_7] \quad (9)$$

where R < 1 and ΔH_7 is the integral enthalpy of solution for reaction 7. The standard enthalpy of formation of KH₂PO₄ is -376.1 kcal mol⁻¹ and that of H₂O is -68.315 kcal mol⁻¹ (9). The standard enthalpies of formation of the KOH solutions were calculated from an equation fitted to published values (10), with a standard deviation of 0.03 kcal (mol of KOH)⁻¹. The standard enthalpies of formation of K₂O-P₂O₅-H₂O solutions where the mole ratios of K₂O:P₂O₅ > 1 were calculated at integers of percent P₂O₅ and percent K₂O by using eq 3, 4, 8, and 9 and are listed in Table V.

Table IV. Integral Enthalpy of Solution of KH_2PO_4 in H_3PO_4 Solutions

			ΔH, kca	l mol ⁻¹
% K 20	% P ₂ O ₅	m_{2}	integral of eq 2	eq 5
$m_1 = 0$	0.510, % P ₂ O	$_{\rm 5} = 3.450 + 1$.40710(% K	(0 ₂ 0)
1.0	4.857	0.2186	5.00	4.96
3.0	7.671	0.6974	4.67	4.63
4.0	9.078	0.9602	4.55	4.56
5.0	10.486	1.2408	4.45	4.45
6.0 7.0	11.893	1.5410	4.36	4.35
7.0		1.0029	4.27	4.20
$m_1 = 1.0$	7.892	s = 6.5/5 + 1 0.2186	.31681(% K 4.95	4 93
2.0	9.209	0.4507	4.77	4.79
3.0	10.525	0.6974	4.63	4.66
4.0	11.842	0.9602	4.51	4.54
6.0	14.476	1.5410	4.33	4.33
7.0	15.793	1.8629	4.25	4.24
8.0	17.109	2.2091	4.16	4.16
$m_1 = 2$	$1.514, \% P_2O$	s = 9.355 + 1	.23649(% 🖡	(₂ 0)
1.0 2.0	10.591	0.2186	4.91 4.75	4.89 4.75
3.0	13.064	0.6974	4.61	4.63
4.0	14.301	0.9602	4.49	4.51
5.0	15.537	1.2408	4.39	4.41
7.0	18.010	1.8629	4.23	4.22
8.0	19.247	2.2091	4.15	4.14
$m_1 = 1$.988, % P ₂ O ₅	= 11.807 + 1	1.16564(%)	K ₂ O)
1.0	12.973	0.2186	4.86	4.84
2.0	14.138	0.4507	4.71 4.58	4.71 4.59
4.0	16.470	0.9602	4.46	4.47
5.0	17.635	1.2408	4.36	4.37
6.0 7.0	18.801	1.5410	4.28	4.27
8.0	21.132	2.2091	4.13	4.19
$m_{2} = 3$.076. % P.O.	= 16.773 + 1	02216(%)	(.0)
1.0	17.795	0.2186	4.70	4.70
2.0	18.817	0.4507	4.58	4.58
3.0 4.0	19.839	0.6974	4.46 4.36	4.46 4.36
5.0	21.884	1.2408	4.27	4.26
6.0	22.906	1.5410	4.19	4.18
7.0	23.928	1.8629	4.11	4.10
9.0	25.972	2.5822	3.98	3.97
$m_{1} = 4$.106, % P.O.	= 20.780 + 0).90639(% I	(,0)
1.0	21.686	0.2186	4.54	4.54
2.0	22.593	0.4507	4.43	4.43
4.0	24.406	0.9602	4.33	4.33
5.0	25.312	1.2408	4.15	4.15
6.0 7.0	26.218	1.5410	4.08	4.07
8.0	28.031	2.2091	3.94	3.94
9.0	28.938	2.5822	3.88	3.89
10.0	29.844	2.9857	3.82	3.85
$m_1 = 5$	$.081, \% P_2O_5$	= 24.075 + 0	.81119(% H	(20)
2.0	24.000 25.697	0.2180	4.37	4.39
3.0	26.509	0.6974	4.19	4.19
4.0	27.320	0.9602	4.11	4.11
5.0 6.0	28.942	1.2408	4.04 3.97	4.03
7.0	29.753	1.8629	3.91	3.90
8.0	30.565	2.2091	3.85	3.85
10.0	32.187	2.9857	3.75	3.77

Table V. Enthalpies of Formation of $K_2O-P_2O_5-H_2O$ Solution, kcal (mol of $P_2O_5)^{-1}$

%			_			% K.	20						
P_2O_5	0	1	2	3	4	5	6	7	8	9	10	11	12
1	619.67	801.59	1109.75	1455.81	1801.69	2147.42	2493.04	2838.57	3184.01	3529.36	3874.60	4219.72	4564.70
2	619.55	712.06	801.92	923.77	1109.76	1282.69	1455.56	1628.38	1801.75	1973.88	2146.57	2319.20	2491.77
3	619.46	681.22	741.87	802.23	862.20	986.07	1109.79	1225.03	1340.24	1455.42	1570.58	1685.70	1800.78
4	619.38	665.75	712.26	757.38	802.52	847.10	924.59	1017.24	1109.84	1196.24	1282.63	1368.99	1455.32
5	619.31	656.44	693.69	731.02	766.75	802.80	838.47	887.83	961.99	1035.97	1109.88	1178.99	1248.07
6	619.24	650.21	681.28	712.44	742.81	773.07	803.05	832.78	863.43	925.24	986.92	1048.46	1109.92
7	619.18	645.75	672.41	699.14	712.92	751.76	759.40	803.29	828.//	854.06	899.03	951.92	1004.70
8	619.12	642.39	665.74	689.14	702.00	730.10	742.50	761.08	803.31 792 70	823.79	873 51	8/9.40	923.71
9 10	619.00	637.66	656 36	675 12	693.92	712.76	731.62	749.87	767.98	785.98	803.89	821 70	839.43
11	618.95	635.92	652.94	670.01	687.12	704.25	721.42	738.59	755.01	771.45	787.79	804.05	820.24
12	618.89	634.47	650.08	665.74	681.44	697.16	712.90	728.66			774.34	789.30	804.20
13	618.84	633.23	647.66	662.12	676.62	691.14	705.69	720.25				776.79	790.59
14	618.78	632.16	645.57	659.02	672.49	685.98	699.50	713.03					778.89
15	618.72	631.23	643.76	656.32	668.90	681.51	694.13	706.76					
16	618.66	630.40	642.16	653.95	665.76	677.58	689.42	701.28					
17	618.60	629.67	640.75	651.86	662.98	674.12	685.27	696.43	707.60				
18	618.54	629.00	639.48	649.99	660.50	6/1.03	681.57	692.12	702.68				
20	618.47	627.95	638.34	646.31	656.20	665 77	675.20	694 79	601 20				
20	618 33	627.34	636 37	645 40	654 45	663.50	672.56	681.63	690.69				
22	618.26	626.88	635.50	644.14	652.79	661.44	670.10	678.76	687.42				
23	618.19	626.44	634.70	642.98	651.26	659.55	667.84	676.13	684.42				
24	618.11	626.03	633.96	641.91	649.86	657.81	665.76	673.72	681.67	689.62			
25	618.03	625.65	633.28	640.91	648.55	656.20	663.85	671.49	679.14	686.78			
26	617.95		632.63	639.99	647.35	654.71	662.07	669.43	676.79	684.14			
27	617.86				646.22	653.32	660.42	667.52	674.61	681.70			
28	617.77					652.02	658.88	665.73	672.58	679.43			
29	617.68						657.44	664.06	6/0.08	675 21			
30	617.39							002.30	000.91	673 11	679 61		
32	617.40									075.44	677.70		
~						% K	.0						
% РО	13	14	15	16	17	18	19	20	21	22	23	24	25
1 205	1000.40	5054.05	5500.02		(205.07	10		20	21		23		
1	4909.49	3234.03	2000 00	3942.29	0283.87	2524 61							
2	2004.23	2030.03	2145 67	2260.46	2275 14	2/29.62							
4	1541.62	1627.88	1714.08	1800.22	1886.27	1972 22	2058.06						
5	1317.13	1386.16	1455.15	1524.09	1592.96	1661.76	1730.47						
6	1167.49	1225.03	1282.54	1340.01	1397.43	1454.80	1512.09						
7	1057.37	1109.94	1159.25	1208.53	1257.77	1306.96	1356.10	1405.16					
8	971.89	1017.99	1064.01	1109.92	1153.02	1196.09	1239.10	1282.06					
9	905.35	946.39	987.36	1028.26	1069.09	1109.84	1148.09	1186.30					
10	857.06	889.06	925.98	962.85	999.66	1036.39	1073.05	1109.68	1144.03				
11	836.35	852.39	875.73	909.28	942.78	976.22	1009.60	1042.91	1076.14				
12	819.03	833.80	848.50	864.61	895.35	926.04	956.67	987.24	1017.75	006 40			
13	804.33	818.01	831.04	845.21	838.12	883.32	911.83	940.08	968.27	996.40			
14	/91.09	702 64	804 52	816 37	878 17	830 07	85163	861 10	923.82	931.90			
16		792.04	793 46	804 60	815.69	826.75	837.76	848 73	859.64	879.60	902.46		
17			,,,,,,,,	794.18	804.65	815.08	825.48	835.84	846.15	856.40	871.26		
18					794.80	804.68	814.53	824.34	834.11	843.83	853.50		
19							804.69	814.01	823.30	832.54	841.74	850.88	
20								804.68	813.53	822.34	831.10	839.82	
21										813.07	821.44	829.77	
22											812.62	820.60	828.53
23													819.79

The solution of KH_2PO_4 in H_3PO_4 solutions can be described by the equation

$$KH_{2}PO_{4} + (y/m_{2})(H_{3}PO_{4} \cdot xH_{2}O) = KH_{2}PO_{4} \cdot (y/m_{2})(H_{3}PO_{4} \cdot xH_{2}O)$$
(10)

where y is the moles of phosphoric acid solution constituting 1000 g of the solvent. The enthalpies of formation of the resultant solutions in kcal (mol of $P_2O_5)^{-1}$ can be determined from the equation

$$\Delta H_t^{\circ}(\text{soln}) = [2(m_2 + y)] \times [m_2 \{\Delta H_t^{\circ}(\text{KH}_2\text{PO}_4) + \Delta H_{10}\} + y \Delta H_t^{\circ}(\text{H}_3\text{PO}_4 \cdot x \text{H}_2\text{O})] (11)$$

where $\Delta {\cal H}_{\rm 10}$ is the integral enthalpy of solution for reaction 10.

The standard enthalpies of formation of the phosphoric acid solutions were calculated from the standard enthalpy of formation of H₃PO₄·100H₂O (-309.7 kcal mol⁻¹) and the enthalpies of solution of orthophosphoric acid. The standard enthalpies of formation of the K₂O-P₂O₅-H₂O solutions where the mole ratio K₂O:P₂O₅ < 1 were calculated at integers of percent P₂O₅ and percent K₂O by using eq 5 and 11 and are listed in Table V.

Densities and Heat Capacities of K20-P205-H20 Solutions

The initial bulk charge of the liquid for each enthalpy of solution measurement was weighed at 25 °C in a modified volumetric flask that had been calibrated with water. From these

Table VI. Density $(g m L^{-1})$ of $K_2 O - P_2 O_5 - H_2 O$ Solutions at 25 °C

						% K ₂ O								
% P ₂ O ₅	0	1	2	3	4	5	6	7	8	9	10	11	12	
$\begin{array}{c} 0\\ 1\\ 2\\ 3\\ 4\\ 5\\ 6\\ 7\\ 8\\ 9\\ 10\\ 11\\ 12\\ 13\\ 14\\ 15\\ 16\\ 17\\ 18\\ 19\\ 20\\ 21\\ 22\\ 23\\ 24\\ 25\\ 26\\ 27\\ 28\\ 29\\ 30\\ 31\\ 32\\ \end{array}$	1.001 1.008 1.015 1.022 1.029 1.036 1.043 1.051 1.059 1.066 1.074 1.082 1.090 1.098 1.107 1.115 1.124 1.132 1.141 1.150 1.159 1.168 1.177 1.186 1.196	$\begin{array}{c} 1.010\\ 1.017\\ 1.024\\ 1.031\\ 1.039\\ 1.046\\ 1.053\\ 1.061\\ 1.069\\ 1.076\\ 1.084\\ 1.092\\ 1.100\\ 1.109\\ 1.117\\ 1.125\\ 1.134\\ 1.143\\ 1.152\\ 1.160\\ 1.170\\ 1.179\\ 1.188\\ 1.197\\ 1.207 \end{array}$	$\begin{array}{c} 1.020\\ 1.027\\ 1.034\\ 1.041\\ 1.049\\ 1.056\\ 1.064\\ 1.071\\ 1.079\\ 1.087\\ 1.095\\ 1.103\\ 1.111\\ 1.119\\ 1.128\\ 1.136\\ 1.145\\ 1.154\\ 1.162\\ 1.171\\ 1.181\\ 1.190\\ 1.199\\ 1.208\\ 1.218\\ 1.228\\ \end{array}$	$\begin{array}{c} 1.030\\ 1.037\\ 1.044\\ 1.052\\ 1.059\\ 1.066\\ 1.074\\ 1.082\\ 1.089\\ 1.097\\ 1.105\\ 1.113\\ 1.122\\ 1.130\\ 1.139\\ 1.147\\ 1.156\\ 1.165\\ 1.174\\ 1.183\\ 1.192\\ 1.201\\ 1.210\\ 1.220\\ 1.220\\ 1.239\\ 1.249 \end{array}$	$\begin{array}{c} 1.041\\ 1.048\\ 1.055\\ 1.062\\ 1.069\\ 1.077\\ 1.085\\ 1.092\\ 1.100\\ 1.108\\ 1.116\\ 1.124\\ 1.133\\ 1.141\\ 1.150\\ 1.158\\ 1.167\\ 1.176\\ 1.185\\ 1.194\\ 1.203\\ 1.213\\ 1.222\\ 1.232\\ 1.241\\ 1.251\\ 1.261\\ 1.271\\ \end{array}$	$\begin{array}{c} 1.051\\ 1.058\\ 1.065\\ 1.073\\ 1.080\\ 1.088\\ 1.095\\ 1.103\\ 1.111\\ 1.119\\ 1.127\\ 1.136\\ 1.144\\ 1.152\\ 1.161\\ 1.170\\ 1.179\\ 1.188\\ 1.197\\ 1.206\\ 1.215\\ 1.224\\ 1.244\\ 1.244\\ 1.253\\ 1.263\\ 1.273\\ 1.283\\ 1.293\\ \end{array}$	$\begin{array}{c} 1.062\\ 1.069\\ 1.076\\ 1.084\\ 1.091\\ 1.099\\ 1.107\\ 1.114\\ 1.122\\ 1.131\\ 1.139\\ 1.147\\ 1.156\\ 1.164\\ 1.173\\ 1.181\\ 1.190\\ 1.199\\ 1.208\\ 1.218\\ 1.227\\ 1.237\\ 1.246\\ 1.256\\ 1.256\\ 1.256\\ 1.256\\ 1.266\\ 1.275\\ 1.285\\ 1.296\\ 1.306\\ \end{array}$	$\begin{array}{c} 1.073\\ 1.080\\ 1.087\\ 1.095\\ 1.102\\ 1.102\\ 1.110\\ 1.118\\ 1.126\\ 1.134\\ 1.142\\ 1.159\\ 1.167\\ 1.159\\ 1.167\\ 1.176\\ 1.185\\ 1.193\\ 1.202\\ 1.211\\ 1.221\\ 1.230\\ 1.239\\ 1.249\\ 1.258\\ 1.268\\ 1.278\\ 1.268\\ 1.278\\ 1.288\\ 1.288\\ 1.308\\ 1.319\\ 1.329 \end{array}$	1.084 1.091 1.099 1.106 1.114 1.122 1.130 1.138 1.146 1.154 1.162 1.171 1.206 1.215 1.224 1.233 1.242 1.252 1.261 1.271 1.281 1.291 1.301 1.311 1.321 1.332 1.342 1.353	1.096 1.103 1.110 1.118 1.126 1.134 1.141 1.150 1.158 1.166 1.174 1.183 1.166 1.174 1.183 1.183 1.183 1.274 1.284 1.294 1.304 1.314 1.324 1.334 1.345 1.355 1.366 1.377	1.107 1.115 1.122 1.130 1.138 1.146 1.154 1.162 1.170 1.178 1.187 1.195 1.204	1.119 1.127 1.134 1.142 1.150 1.158 1.166 1.174 1.182 1.191 1.199 1.208 1.217 1.225	1.131 1.139 1.147 1.154 1.162 1.170 1.178 1.187 1.195 1.204 1.212 1.221 1.230 1.239 1.248	_
<u> </u>						% K ₂ O				·····		···· · · · ·		-
% P2O5	13	14	15	16	17	18	19	20	21	22	23	24	25	
0 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23	1.144 1.152 1.159 1.167 1.175 1.183 1.191 1.200 1.208 1.217 1.225 1.234 1.243 1.252 1.261 1.270	1.157 1.164 1.172 1.180 1.188 1.196 1.204 1.213 1.221 1.230 1.238 1.247 1.256 1.265 1.274 1.284	$\begin{array}{c} 1.170\\ 1.177\\ 1.185\\ 1.193\\ 1.201\\ 1.209\\ 1.218\\ 1.226\\ 1.235\\ 1.243\\ 1.252\\ 1.261\\ 1.270\\ 1.279\\ 1.288\\ 1.298\\ 1.307\\ \end{array}$	1.183 1.191 1.198 1.206 1.215 1.223 1.231 1.240 1.248 1.257 1.266 1.275 1.284 1.293 1.302 1.312 1.321 1.331	1.196 1.204 1.212 1.220 1.228 1.237 1.245 1.254 1.262 1.271 1.280 1.289 1.298 1.307 1.317 1.326 1.336 1.345 1.355	$\begin{array}{c} 1.210\\ 1.218\\ 1.226\\ 1.234\\ 1.242\\ 1.251\\ 1.259\\ 1.268\\ 1.276\\ 1.285\\ 1.294\\ 1.303\\ 1.312\\ 1.322\\ 1.321\\ 1.341\\ 1.350\\ 1.360\\ 1.370\\ \end{array}$	1.256 1.265 1.273 1.282 1.291 1.300 1.309 1.318 1.327 1.336 1.346 1.346 1.355 1.365 1.375 1.385 1.395	1.297 1.305 1.314 1.323 1.333 1.342 1.351 1.361 1.370 1.380 1.390 1.400 1.410 1.420	1.338 1.348 1.357 1.366 1.376 1.386 1.396 1.405 1.416 1.426 1.436 1.446	1.382 1.392 1.401 1.411 1.421 1.431 1.441 1.452 1.462	1.427 1.437 1.447 1.457 1.468 1.478 1.489	1.474 1.484 1.495 1.505	1.522	_

weights the densities in g mL^{-1} , d, of the solutions were determined. The equation

d = 1.0008 + 0.006761P + 0.009439K +

$$0.0000567P^2 + 0.0001207K^2 + 0.0000613PK$$
 (12)

fits the observed data, with a standard deviation of 0.004 g mL⁻¹. The concentrations of the solutions, the observed densities, and those calculated from eq 12 are listed in the supplementary material. Equation 12 was used to calculate the densities at integers of percent P₂O₅ and percent K₂O (Table VI).

The total weight of solution in the calorimeter, the temperature rise, and the electrical energy input during the second electrical calibration for each measurement made possible the determination of the heat capacity, s, in cal $g^{-1} \circ C^{-1}$ for each solution at the average temperature of the calibration. The water equivalent of the calorimeter had been determined previously. The equation

 $s = 0.9847 - 0.008699P - 0.012670K - 0.0000287P^{2} + 0.0000153K^{2} + 0.0002159PK$ (13)

Table VII. Heat Capacity (cal g⁻¹ °C⁻¹) of K₂O-P₂O₅-H₂O Solutions at 25 °C

						% K 20								
$\% P_2O_5$	0	1	2	3	4	5	6	7	8	9	10	11	12	
$\begin{array}{c} 0\\ 1\\ 2\\ 3\\ 4\\ 5\\ 6\\ 7\\ 8\\ 9\\ 10\\ 11\\ 12\\ 13\\ 14\\ 15\\ 16\\ 17\\ 18\\ 19\\ 20\\ 21\\ 22\\ 23\\ 24\\ 25\\ 26\\ 27\\ 28\\ 29\\ 30\\ 31\\ 32\\ \end{array}$	0.985 0.976 0.967 0.958 0.949 0.940 0.931 0.922 0.913 0.904 0.895 0.867 0.857 0.848 0.857 0.848 0.828 0.819 0.779 0.769 0.759	0.972 0.964 0.955 0.946 0.938 0.929 0.920 0.911 0.902 0.893 0.884 0.875 0.866 0.857 0.848 0.829 0.820 0.810 0.791 0.781 0.772 0.752	0.959 0.951 0.943 0.934 0.926 0.917 0.909 0.900 0.891 0.883 0.874 0.865 0.874 0.865 0.847 0.838 0.829 0.820 0.811 0.792 0.783 0.773 0.764 0.754 0.735	0.947 0.939 0.931 0.922 0.914 0.906 0.897 0.889 0.881 0.872 0.863 0.855 0.846 0.837 0.828 0.820 0.811 0.802 0.774 0.765 0.756 0.746 0.718	0.934 0.926 0.918 0.910 0.902 0.894 0.886 0.878 0.870 0.861 0.853 0.845 0.836 0.828 0.810 0.802 0.793 0.784 0.775 0.766 0.757 0.748 0.730 0.720 0.711 0.702	0.922 0.914 0.906 0.899 0.891 0.883 0.875 0.859 0.859 0.851 0.843 0.834 0.826 0.818 0.801 0.792 0.784 0.775 0.767 0.758 0.749 0.740 0.722 0.713 0.704 0.695 0.686	0.909 0.902 0.894 0.871 0.864 0.856 0.840 0.832 0.824 0.832 0.824 0.808 0.808 0.792 0.783 0.775 0.767 0.758 0.775 0.767 0.758 0.7724 0.715 0.706 0.697 0.688 0.679	0.897 0.890 0.882 0.875 0.868 0.860 0.853 0.845 0.837 0.830 0.822 0.814 0.806 0.798 0.790 0.792 0.774 0.766 0.758 0.750 0.741 0.733 0.725 0.716 0.708 0.699 0.682 0.664	0.884 0.877 0.870 0.863 0.856 0.849 0.841 0.834 0.827 0.812 0.812 0.804 0.773 0.765 0.757 0.749 0.741 0.733 0.725 0.717 0.709 0.692 0.684 0.675 0.667 0.658 0.649	0.872 0.865 0.858 0.851 0.844 0.837 0.830 0.823 0.816 0.809 0.801 0.794 0.794 0.709 0.701 0.693 0.669 0.660 0.652 0.643 0.635	0.859 0.853 0.846 0.840 0.833 0.826 0.819 0.812 0.798 0.791 0.784 0.777 0.784 0.777 0.662 0.654 0.646 0.637 0.629	0.847 0.841 0.834 0.828 0.821 0.815 0.808 0.795 0.788 0.774 0.767 0.760	0.835 0.829 0.822 0.816 0.810 0.804 0.797 0.791 0.778 0.771 0.764 0.757 0.751 0.744	
% P O	13	14	15	16	17	18	19	20	21	22	23	24	25	
0 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23	0.823 0.817 0.811 0.805 0.799 0.792 0.786 0.780 0.774 0.761 0.754 0.748 0.748 0.748 0.734 0.728	$\begin{array}{c} 0.810\\ 0.805\\ 0.799\\ 0.793\\ 0.787\\ 0.781\\ 0.769\\ 0.763\\ 0.757\\ 0.763\\ 0.757\\ 0.751\\ 0.744\\ 0.738\\ 0.732\\ 0.725\\ 0.719\\ \end{array}$	0.798 0.793 0.781 0.776 0.770 0.764 0.758 0.753 0.747 0.741 0.741 0.728 0.722 0.716 0.703	$\begin{array}{c} 0.786\\ 0.781\\ 0.775\\ 0.775\\ 0.770\\ 0.764\\ 0.759\\ 0.753\\ 0.748\\ 0.742\\ 0.736\\ 0.742\\ 0.736\\ 0.731\\ 0.725\\ 0.719\\ 0.713\\ 0.707\\ 0.701\\ 0.695\\ 0.688\\ \end{array}$	$\begin{array}{c} 0.774\\ 0.769\\ 0.764\\ 0.753\\ 0.753\\ 0.748\\ 0.742\\ 0.737\\ 0.732\\ 0.726\\ 0.721\\ 0.715\\ 0.709\\ 0.703\\ 0.698\\ 0.692\\ 0.686\\ 0.680\\ 0.674\\ \end{array}$	$\begin{array}{c} 0.762\\ 0.757\\ 0.757\\ 0.752\\ 0 & ??7\\ (x 42\\ 0/37\\ 0.732\\ 0.726\\ 0.721\\ 0.716\\ 0.711\\ 0.705\\ 0.700\\ 0.694\\ 0.689\\ 0.683\\ 0.677\\ 0.671\\ 0.666\end{array}$	$\begin{array}{c} 0.731\\ 0.726\\ 0.721\\ 0.716\\ 0.711\\ 0.706\\ 0.701\\ 0.695\\ 0.695\\ 0.699\\ 0.685\\ 0.679\\ 0.663\\ 0.657\\ 0.652\\ \end{array}$	0.705 0.700 0.696 0.681 0.676 0.665 0.665 0.660 0.655 0.649 0.644 0.638	0.681 0.676 0.671 0.666 0.651 0.646 0.641 0.636 0.631 0.625	0.657 0.652 0.648 0.643 0.638 0.633 0.628 0.623 0.618	0.634 0.630 0.625 0.620 0.615 0.610 0.605	0.612 0.608 0.603 0.598	0.591 0.586	

fits the observed data, with a standard deviation of 0.003 cal g^{-1} °C⁻¹. The concentrations of the solutions, the average temperature of each measurement, the observed heat capacities, and those calculated from eq 13 are listed in the supplementary material. Equation 13 was used to calculate the heat capacities at integers of percent $\mathsf{P}_2\mathsf{O}_5$ and percent $\mathsf{K}_2\mathsf{O}$ (Table VII). The average temperature of all the observed heat capacities is 25.7 °C, with a standard deviation of 0.4 °C; but since the rate of change of heat capacity with temperature is small, no corrections were applied to convert the heat capacities to 25 °C.

Registry No. Potassium dihydrogen orthophosphate, 7778-77-0; potassium hydroxide, 1310-58-3; orthophosphoric acid, 7664-38-2.

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Supplementary Material Available: Tables of differential enthalpies, integral enthalpies, observed and calculated densities, and observed and calculated heat capacities (33 pages) are included in the supplementary material. Ordering information is given on any current masthead page.

Salting Effects of p-Aminophenol in Some Protic Solvents at 20 °C

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Saturation solubilities of *p*-aminophenol (PAP) in the presence of four salts, viz., NaCl, Na₂SO₄, NaClO₄, and KSCN, in three solvents, viz., water, ethyl acetate, and dioxane, have been determined at 20 °C. The effect of satts on the solubility of *p*-aminophenol and the satting coefficients, K_{s} , have been evaluated. The salting out decreases in the order Na₂SO₄ > NaCl > NaClO₄ > KSCN. Dioxane shows the highest salting order followed by ethyl acetate and water.

Introduction

The process of salting out is studied by shaking a solute between two immiscible solvent phases, one of them being the organic phase and the other the aqueous phase containing the salt called the salting-out agent, and then analyzing the solute concentration in one phase or both phases. However, if the information desired relates to miscible solvents, the ratio of solubilities in two separate solvents is measured and reported as the distribution coefficient. Furthermore, when protic solvents are used for salting studies, as in the present case, the ratio of the saturation solubility of the solute in pure solvent and in the presence of salt can be used to calculate the salting-out coefficient.

The solubility method has been used extensively to study the salting effect for various classes of organic compounds. Amino acids (1, 2), phenols and cresols (3), toluene (4), benzoyltri-fluoroacetone (5), hydrocarbons and substituted benzenes (6), monoalkylbenzene (7), etc., in the presence of salting agents have been studied by the solubility method. The solubility technique, however, requires relatively high concentrations of organic solutes to saturate many solvents.

We have determined the saturation solubilities of p-aminophenol (hereafter designated PAP) in the presence of four salts (both structure makers and structure breakers), viz., sodium chloride (NaCl), sodium sulfate (Na₂SO₄), sodium perchlorate (NaClO₄), and potassium thiocyanate (KSCN), in three protic solvents, viz., water, dioxane, and ethyl acetate, at 20 °C. The solubility technique was utilized here, due to the reason that PAP is almost insoluble in aprotic solvents (like benzene, toluene, etc.) and the extraction technique was not suitable for the present studies.

Experimental Section

E. Merck AnalaR-grade PAP was vacuum dried over anhydrous NaOH to remove any existing traces of water. All salts, viz., NaCl, Na₂SO₄, NaClO₄, and KSCN, were of AnalaR grade and were used without any further purification. Dioxane and ethyl acetate of BDH AnalaR grade and water were double distilled at temperatures much below their boiling points at a recovery rate of 1.0 mL min⁻¹.

Saturation solubilities of PAP in the absence and the presence of weighed amounts of salts in different solvents were calculated. Different amounts of salt required for different molarities (from 0.2 to 2 M) for a fixed volume of solvent were shaken along with excess PAP in stoppered Corning-glass boiling tubes for about 6 h to obtain saturation with respect to PAP. After being shaken, the solutions were set aside for several hours, or until the solutions became clear. A thermostatic shaker with an arrangement for holding as many as 18 boiling tubes was used for shaking. This maintained the temperature to ± 0.2 °C.

A Carl Zeiss Specord UV-vis spectrophotometer with a thermostated cell compartment and 5.0- and 1.0-cm and 1.0-mm matched quartz cells were used for absorbance measurements.

The clear solution of PAP obtained after shaking was separated (diluted where required) and its absorbance noted in the UV region at 312 nm. The concentration was found from the known values, as the Beer–Lambert law was found to be valid. The precision in all cases was better than 1.0%. The reproducible values only have been recorded in Table I.

Results and Discussion

The salting coefficient, K_s , is most commonly determined from the solubility according to the empirical Setschenow equation (β)

$$\log f = \log \left(S^{\circ} / S \right) = K_{s} C_{s} \tag{1}$$

where S^0 and S denote the solubility of PAP in pure solvent and in the presence of salt, respectively, C_s is the salt concentration, and f is the activity coefficient of PAP in the solvent when salt is added. The plot of log (S^0/S) against C_s gave straight